## Gas Supply Design Guide

## CFR Boilers

Models CFR1500 and CFR3000

Other documents for this product include:
TAG-0105 CFR Boiler Vent \& Combustion Air Guide
TAG-0107 CFR Boiler Application Guide
TAG-0108 CFR Boiler Electrical Guide


## Disclaimer

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## 1. SAFETY PRECAUTIONS

AERCO CFR boilers are modulating input devices that require an adequate volume of natural gas at constant pressure for proper operation. The gas requirements specified in this document must be satisfied to ensure efficient combustion. Designers and installers must adhere to the AERCO specifications and those of the local authorities having jurisdiction. A thorough understanding and knowledge of these guidelines is required for the successful design and installation of CFR boilers.

### 1.1 Gas Train Components

AERCO CFR boilers are equipped with standard UL approved/FM compliant gas trains. These gas trains are factory tested and fired, with a minimum number of modular components. The gas train components have been designed to operate at high combustion efficiencies by closely controlling both the volume and air/fuel mixture to the burner. The major internal gas train components are:

* SAFETY SHUT OFF VALVE (SSOV) With BUILT-IN SUPPLY GAS REGULATOR - An electrohydraulic gas valve, containing a proof of closure switch, is utilized to stop fuel from flowing into the gas train of the boiler. This is a $100 \%$ tight shutoff device with a visible window indicator showing valve position. Reliable, and a standard industry component, this valve is factory piped with a low gas pressure switch on the inlet side of the valve which monitors the manifold pressure for minimum supply conditions. There is also a high gas pressure switch installed on the outlet side of the gas valve, which shuts down the boiler if gas manifold pressures exceed maximum conditions.
For minimum and maximum gas pressures, see Table 1, below.
* AIR/FUEL VALVE - The air/fuel valve controls the volume and mixture of air and fuel in perfect proportion throughout the entire modulation range of the boiler. The valve utilizes one common shaft to simultaneously vary the gas port area and air volume. The gas portion of the valve is a slide port type valve with linear proportion-to-position characteristics. The air side uses a butterfly type valve for adjusting the air volume. The driver of the valve shaft is a precision stepping motor which provides continuous positioning from full input to minimum fire. The air/fuel valve also contains two proof-of-position switches.
* CAST ALUMINUM BLOWER ASSEMBLY - A cast aluminum pre-mix blower ensures the precise mixing of air and fuel prior to entering the burner thereby providing controlled combustion.
* LOW NOx BURNER - The burner provides the actual point of air/fuel contact and combustion into the cylindrical combustion/heat exchanger. Fabricated from metal fiber mesh covering a stainlesssteel body, the burner is stable throughout the entire input range of the boiler. The spark igniter and flame detector for the combustion supervision system are part of this assembly. The burner is easily removable from the boiler.


## 2. GAS PRESSURE REQUIREMENTS

AERCO CFR boilers require a stable natural gas input pressure. A low supply gas pressure switch in each gas train prevents the boiler from operating without sufficient pressure. The allowable gas inlet pressure range when firing at maximum input is shown in Table 1.

TABLE 1: Allowable Gas Inlet Pressure for Standard Gas Trains

| Model | NATURAL GAS |  |
| :--- | :---: | :---: |
|  | Minimum | Maximum |
| CFR1500 | $4.0^{\prime \prime}$ W.C. $(1.00 \mathrm{kPa})$ | $14.0^{\prime \prime}$ W.C. $(3.49 \mathrm{kPa})$ |
| CFR3000 | $4.0^{\prime \prime}$ W.C. $(1.00 \mathrm{kPa})$ | $14.0^{\prime \prime}$ W.C. $(3.49 \mathrm{kPa})$ |

Gas pressure must be measured when the unit is in operation (firing). Measure the gas pressure with a manometer at the NPT ball valve provided at the SSOV inlet. In a multiple boiler installation, gas pressure must initially be set for single boiler operation, and then the remaining boilers must be staged on at full fire, to insure gas pressures never falls below the supply gas pressure when the single unit was firing.
All CFR models have a low supply gas pressure switch in the gas train to prevent operation if incoming gas pressure is insufficient.

### 2.1 Isolation Valves

A manual shutoff valve must be installed in each boiler, as shown in Figure 2-1. This valve is supplied with the boiler.

### 2.2 Pressure Regulators

The lock-up type pressure regulator(s) must be sized as follows:
TABLE 2: Lock-Up Regulator Sizing

| Boiler Size (MBH) | CFH | $\left.\mathbf{( m}^{3} / \mathbf{H R}\right)$ |
| :---: | :---: | :---: |
|  | $1500-1750$ | $(42.5-49.6)$ |
| CFR1500 | $3000-3400$ | $(85.0-96.3)$ |

An external lock-up type regulator MUST be installed downstream of the isolation valve at all installations where gas supply pressure will exceed 14.0" W.C. (3.49 kPa).
External gas regulators are self-contained with tapped diaphragm vent ports allowing the diaphragm to change its position as required. These vents typically require piping to the outside. For details, see Section 7: Venting of Gas Supply Regulators, below. The SSOV/Regulator in the gas train is factory piped and does not require any vent piping.

CAUTION:
AERCO boilers must be isolated from the system when leak testing.

Drip legs are typically required at the gas supply of each boiler to prevent any dirt, weld slag, or debris from entering the boiler gas train inlet pipe. When multiple boilers are installed, some utilities and local codes require a full-size drip leg on the main gas supply line in addition to the drip leg at each unit. The bottom of the gas drip leg(s) should be removable without disassembling any gas piping. The weight of the gas pipe must not be supported from the bottom of the drip leg. The drip leg(s) must not be used to support any or part of the gas piping.

On all CFR models it is strongly recommended that the pressure regulator be installed a minimum distance of 10 pipe diameters between the pressure regulator and the nearest downstream fittings (an elbow or the unit itself), and a minimum of 5 pipe diameters between the pressure regulator and any upstream fitting, such as elbow or shutoff valve, as shown below. This recommendation applies to all gas trains on all CFR Boiler models.

NOTE: It is the responsibility of the customer to source and purchase the appropriate gas regulator as described above. However, AERCO offers for sale an appropriate regulator, which may be ordered at the time of unit purchase or separately. Contact your AERCO sales representative for more information.


Figure 2-1: CFR1500 \& CFR3000 Gas Regulator and Manual Shut-Off Valve

### 2.3 Massachusetts Installations Only

For Massachusetts installations, a mandatory external gas supply regulator must be positioned as shown above. The gas supply regulator must be properly vented to outdoors. Consult the local gas utility for detailed requirements concerning venting of the supply gas regulator.

### 2.4 Multiple Unit Installations

The following points apply to sites that have multiple CFR units installed:

- If inlet pressures are above $\mathbf{7 "}$ W.C. ( 1.74 kPa ) a gas pressure regulator may be highly recommended, based on site conditions. Consult your AERCO representative or the factory.
- If inlet pressures are above 14 " W.C. $(\mathbf{3 . 4 9} \mathbf{~ k P a})$ a gas pressure regulator is mandatory.

The following are AERCO's recommendations for installation of gas pressure regulator, unless superseded by state and local codes and the regulator manufacturer's specifications:

- Horizontal installation of gas pressure regulators is recommended unless stated otherwise by the regulator manufacturer. Consult the manufacturer for additional recommendations and installation options.
- When installed horizontally, the required distance between the gas pressure regulator and the nearest pipe fitting, elbow or valve is 10 pipe diameters, as shown in Figure 2-1.
- When pipe size reduction is required, use only bell reducers.


## 3. GAS PIPING

All gas piping and components must comply with NFPA local codes, and utility requirements minimum. Only gas approved fittings, valves, or pipe should be utilized.
Standard industry practice for gas piping is Schedule 40 iron pipe and fittings. All high and low gas pressure piping systems must comply with local utility and building codes.

Assembled piping must be clean of all debris, pipe chips and foreign material to prevent any from entering the boiler's gas train. Piping must be tested as prescribed in NFPA 54. Equipment must be isolated before testing any piping system over the allowable pressure. DO NOT EXCEED 14.0" W.C. $(3.49 \mathrm{kPa})$ on the inlet side of the CFR boiler at any time.

The diameter of the gas inlet pipes is as follows:

| Inlet Pipe Diameter |  |
| :--- | :---: |
| CFR Model | Natural Gas |
|  |  |
| 1500 | 2 Inch |
| 3000 | 2 Inch |

## 4. GAS SUPPLY MAIN SIZING

Gas pipe sizing, for either a single or multiple boiler installation, must be sized for a maximum pressure drop of 0.3" W.C. ( 75 Pa ) from the source to the final boiler. The maximum gas flow rate required is the sum of the maximum inputs of each unit divided by the heat of combustion of the fuel supplied at the location, (approximately 1,030 BTU per cubic foot [ 38.35 megajoule/cubic meter] of natural gas). The fuel supplier or utility should be consulted to confirm that sufficient volume and normal pressure is provided to the building at the discharge side of the gas meter or supply pipe. For existing installations with gas equipment, gas pressure must be measured with a manometer to be certain sufficient pressure is available. Before sizing gas piping, a survey of all connected gas devices must be made. Gas piping supplying more than one gas device must be able to handle the total connected input within the allowable gas pressure drop. The allowable minimum and maximum gas pressure for each device must be considered. Whenever the minimum and maximum gas pressures vary between devices, gas pressure regulators at each unit must be installed to allow regulation at any individual unit. Gas pressure must never exceed the maximum allowable rating of any connected device.

The total length of gas piping as well as fitting pressure drop must be considered when sizing the gas piping. Total equivalent length must be calculated from the meter or source location to the last boiler connected on the header. The values in the Gas Piping Tables 4,5 and 6 (in Section 6) which contain data extracted from NFPA 54, must be used as a minimum guideline. Gas pipe size must be selected on the total equivalent length from the appropriate pressure table. The gas volume for CFH ( $\mathrm{m}^{3} / \mathrm{hr}$.) flow will be the input divided by the calorific value of the fuel to be supplied.

## 5. GAS HEADER SIZING

Main supply gas pipe sizing must be developed for the total plant. Boiler gas manifold piping must be sized based on the volume requirements and lengths between boilers and the fuel main. Header sizes can be either full size or stepped in size as units are connected. A typical gas piping header diagram for a 4-module CFR Boiler Plant is illustrated in Figure 3.


Figure 3-1: Typical Multiple Boiler Manifold Construction

* Based on Table 4 on the following pages for natural gas, 0.6 specific gravity, 1,000 CFH (28 $\mathrm{m}^{3} / \mathrm{hr}$.) / unit, actual header sizes will vary with length of pipe run and fittings employed.

If supply gas pressure exceeds $\mathbf{1 4 . 0}$ " W.C. ( $\mathbf{3 . 4 9} \mathbf{~ k P a}$ ), a single lock-up regulator in the header, or individual lock-up regulators in each unit must be used to bring the gas pressure down to 14.0" W.C. ( $3.49 \mathbf{k P a}$ ). The header should be located above or behind boiler. Gas piping should not be installed directly over top or front of any part of boiler. Sufficient clearances for maintenance are required.

## 6. GAS PIPING TABLES

The data in the following pipe and vent sizing tables have been extracted from the National Fire Protection Association Article 54 (NFPA 54).

TABLE 4: Maximum Capacity of Pipe for 0.5 PSI or Less (Imperial Units)
In Cubic Feet of Gas per Hour
For a Pressure Drop of 0.3-inch Water Column

| Nominal Iron Pipe Size in Inches | Internal Diameter in Inches | Total Equivalent Length of Pipe (Feet) |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 | 90 | 125 | 150 | 175 | 200 |
| 2.00 | 2.067 | 3,050 | 2,100 | 1,650 | 1,450 | 1,270 | 1,150 | 1,050 | 990 | 930 | 780 | 710 | 650 | 610 |
| 2.50 | 2.469 | 4,800 | 3,300 | 2,700 | 2,300 | 2,000 | 1,850 | 1,700 | 1,600 | 1,500 | 1,250 | 1,130 | 1,050 | 980 |
| 3.00 | 3.068 | 8,500 | 5,900 | 4,700 | 4,100 | 3,600 | 3,250 | 3,000 | 2,800 | 2,600 | 2,200 | 2,000 | 1,850 | 1,700 |
| 4.00 | 4.026 | 17,500 | 12,000 | 9,700 | 8,300 | 7,400 | 6,800 | 6,200 | 5,800 | 5,400 | 4,500 | 4,100 | 3,800 | 3,500 |

TABLE 4: Maximum Capacity of Pipe for 3.45 kPa or Less (Metric Units)
In Cubic Meters of Gas per Hour ( $\mathrm{m}^{3} / \mathrm{hr}$.)
For a Pressure Drop of 75 Pa

| Nominal Iron Pipe Size in mm | Internal Diam. in mm | Total Equivalent Length of Pipe (Meters) |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 3.05 | 6.1 | 9.14 | 12.19 | 15.24 | 18.28 | 21.33 | 24.38 | 27.43 | 38.1 | 45.72 | 53.34 | 60.96 |
| 50.80 | 52.50 | 86.37 | 59.47 | 46.72 | 41.06 | 35.96 | 32.56 | 29.73 | 28.03 | 26.33 | 22.09 | 20.10 | 18.41 | 17.27 |
| 63.50 | 62.71 | 135.92 | 93.45 | 76.46 | 65.13 | 56.63 | 52.39 | 48.14 | 45.31 | 42.48 | 35.40 | 32.00 | 29.73 | 27.75 |
| 76.20 | 77.93 | 240.69 | 167.07 | 133.09 | 116.10 | 101.94 | 92.03 | 84.95 | 79.29 | 73.62 | 62.30 | 56.63 | 52.39 | 48.14 |
| 101.60 | 102.26 | 495.54 | 339.80 | 274.67 | 235.03 | 209.54 | 192.55 | 175.56 | 164.24 | 152.91 | 127.43 | 116.10 | 107.60 | 99.11 |

TABLE 5: Pipe Sizing Table for 1 Pound Pressure (Imperial Units)
Capacity of Pipes of Different Diameters and Lengths
In Cubic Feet per Hour with a 10\% Pressure Drop and a Gas of 0.6 Specific Gravity

| Pipe Size of Schedule 40 Standard Pipe in Inches | Internal Diameter in Inches | Total Equivalent Length of Pipe (Feet) |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 50 | 100 | 150 | 200 | 250 | 300 | 400 | 500 |
| 2.00 | 2.067 | 4245 | 2918 | 2343 | 2005 | 1777 | 1610 | 1378 | 1222 |
| 2.50 | 2.469 | 6766 | 4651 | 3735 | 3196 | 2833 | 2567 | 2197 | 1947 |
| 3.00 | 3.068 | 11962 | 8221 | 6602 | 5650 | 5008 | 4538 | 3884 | 3442 |
| 3.50 | 3.548 | 17514 | 12037 | 9666 | 8273 | 7332 | 6644 | 5686 | 5039 |
| 4.00 | 4.026 | 24398 | 16769 | 13466 | 11525 | 10214 | 9255 | 7921 | 7020 |
| 5.00 | 5.047 | 44140 | 30337 | 24362 | 20851 | 18479 | 16744 | 14330 | 12701 |
| 6.00 | 6.065 | 71473 | 49123 | 39447 | 33762 | 29923 | 27112 | 23204 | 20566 |
| 8.00 | 7.981 | 146849 | 100929 | 81049 | 69368 | 61479 | 55705 | 47676 | 42254 |

## TABLE 5: Pipe Sizing Table for for 6.89 kPa Pressure: (Metric Units)

Capacity of Pipes of Different Diameters and Lengths
In Cubic Meters per Hour with a 10\% Pressure Drop and a Gas of 0.6 Specific Gravity

| Pipe Size of Schedule 40 Standard Pipe in mm | Internal Diam. in mm | Total Equivalent Length of Pipe (Meters) |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 15.24 | 30.48 | 45.72 | 60.96 | 76.2 | 91.44 | 121.92 | 152.4 |
| 50.80 | 52.50 | 120.21 | 82.63 | 66.35 | 56.78 | 50.32 | 45.59 | 39.02 | 34.60 |
| 63.50 | 62.71 | 191.59 | 131.70 | 105.76 | 90.50 | 80.22 | 72.69 | 62.21 | 55.13 |
| 76.20 | 77.93 | 338.73 | 232.79 | 186.95 | 159.99 | 141.81 | 128.50 | 109.98 | 97.47 |
| 88.90 | 90.12 | 495.94 | 340.85 | 273.71 | 234.27 | 207.62 | 188.14 | 161.01 | 142.69 |
| 101.60 | 102.26 | 690.88 | 474.85 | 381.32 | 326.35 | 289.23 | 262.07 | 224.30 | 198.79 |
| 127.00 | 128.19 | 1249.91 | 859.05 | 689.86 | 590.44 | 523.27 | 474.14 | 405.78 | 359.65 |
| 152.40 | 154.05 | 2023.90 | 1391.02 | 1117.02 | 956.04 | 847.33 | 767.73 | 657.07 | 582.37 |
| 203.20 | 202.72 | 4158.32 | 2858.01 | 2295.06 | 1964.29 | 1740.90 | 1577.40 | 1350.04 | 1196.51 |

TABLE 6: Pipe Sizing Table for an Initial Pressure of 2.0 PSI (Imperial Units)
Capacity of Pipes of Different Diameters and Lengths
In Cubic Feet per Hour with a $10 \%$ Pressure Drop and a Gas of 0.6 Specific Gravity

| Pipe Size of Schedule 40 Standard Pipe in Inches | Internal Diameter in Inches | Total Equivalent Length of Pipe (Feet) |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 50 | 100 | 150 | 200 | 250 | 300 | 400 | 500 |
| 2.00 | 2.067 | 6589 | 4528 | 3636 | 3112 | 2758 | 2499 | 2139 | 1896 |
| 2.50 | 2.469 | 10501 | 7217 | 5796 | 4961 | 4396 | 3983 | 3409 | 3022 |
| 3.00 | 3.068 | 18564 | 12759 | 10246 | 8769 | 7772 | 7042 | 6027 | 5342 |
| 3.50 | 3.548 | 27181 | 18681 | 15002 | 12840 | 11379 | 10311 | 8825 | 7821 |
| 4.00 | 4.026 | 37865 | 26025 | 20899 | 17887 | 15853 | 14364 | 12293 | 10895 |
| 5.00 | 5.047 | 68504 | 47082 | 37809 | 32359 | 28680 | 25986 | 22240 | 19711 |
| 6.00 | 6.065 | 110924 | 76237 | 61221 | 52397 | 46439 | 42077 | 36012 | 31917 |

TABLE 6: Pipe Sizing Table for an Initial Pressure of 13.79 kPa: (Metric Units)
Capacity of Pipes of Different Diameters and Lengths
In Cubic Feet per Hour with a 10\% Pressure Drop and a Gas of 0.6 Specific Gravity

| Pipe Size of Schedule 40 Standard Pipe in mm | Internal Diameter in mm | Total Equivalent Length of Pipe (Meters) |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 15.24 | 30.48 | 45.72 | 60.96 | 76.2 | 91.44 | 121.92 | 152.4 |
| 50.80 | 52.50 | 186.58 | 128.22 | 102.96 | 88.12 | 78.10 | 70.76 | 60.57 | 53.69 |
| 63.50 | 62.71 | 297.36 | 204.36 | 164.13 | 140.48 | 124.48 | 112.79 | 96.53 | 85.57 |
| 76.20 | 77.93 | 525.68 | 361.30 | 290.14 | 248.31 | 220.08 | 199.41 | 170.67 | 151.27 |
| 88.90 | 90.12 | 769.68 | 528.99 | 424.81 | 363.59 | 322.22 | 291.98 | 249.90 | 221.47 |
| 101.60 | 102.26 | 1072.22 | 736.95 | 591.80 | 506.51 | 448.91 | 406.75 | 348.10 | 308.51 |
| 127.00 | 128.19 | 1939.83 | 1333.22 | 1070.64 | 916.31 | 812.13 | 735.85 | 629.77 | 558.16 |
| 152.40 | 154.05 | 3141.03 | 2158.80 | 1733.60 | 1483.73 | 1315.01 | 1191.49 | 1019.75 | 903.79 |

TABLE 7: Pipe Sizing Table for an Initial Pressure of 5.0 PSI (Imperial Units)
Capacity of Pipes of Different Diameters and Lengths
In Cubic Feet per Hour with a 10\% Pressure Drop and a Gas of 0.6 Specific Gravity

| Pipe Size of Schedule 40 Standard Pipe in Inches | Internal Diameter in Inches | Total Equivalent Length of Pipe (Feet) |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 15.24 | 30.48 | 45.72 | 60.96 | 76.2 | 91.44 | 121.92 | 152.4 |
| 2.00 | 2.067 | 11786 | 8101 | 6505 | 5567 | 4934 | 4471 | 3827 | 3391 |
| 2.50 | 2.469 | 18785 | 12911 | 10368 | 8874 | 7865 | 7126 | 6099 | 5405 |
| 3.00 | 3.068 | 33209 | 22824 | 18329 | 15687 | 13903 | 12597 | 10782 | 9556 |
| 3.50 | 3.548 | 48623 | 33418 | 26836 | 22968 | 20365 | 18444 | 15786 | 13991 |
| 4.00 | 4.026 | 67736 | 46555 | 37385 | 31997 | 28358 | 25694 | 21991 | 19490 |
| 5.00 | 5.047 | 122544 | 84224 | 67635 | 57887 | 51304 | 46485 | 39785 | 35261 |
| 6.00 | 6.065 | 198427 | 136378 | 109516 | 93732 | 83073 | 75270 | 64421 | 57095 |

TABLE 7: Pipe Sizing Table for an Initial Pressure of $\mathbf{3 4 . 4 7}$ kPa: (Metric Units)
Capacity of Pipes of Different Diameters and Lengths
In Cubic Feet per Hour with a 10\% Pressure Drop and a Gas of 0.6 Specific Gravity

| Pipe Size of <br> Schedule 40 <br> Standard Pipe in mm | Internal Diameter in mm | Total Equivalent Length of Pipe (Meters) |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 15.24 | 30.48 | 45.72 | 60.96 | 76.2 | 91.44 | 121.92 | 152.4 |
| 50.80 | 52.50 | 333.74 | 229.40 | 184.20 | 157.64 | 139.72 | 126.61 | 108.37 | 96.02 |
| 63.50 | 62.71 | 531.93 | 365.60 | 293.59 | 251.29 | 222.71 | 201.79 | 172.71 | 153.05 |
| 76.20 | 77.93 | 940.38 | 646.31 | 519.02 | 444.21 | 393.69 | 356.71 | 305.31 | 270.60 |
| 88.90 | 90.12 | 1376.86 | 946.30 | 759.92 | 650.38 | 576.68 | 522.28 | 447.01 | 396.18 |
| 101.60 | 102.26 | 1918.08 | 1318.30 | 1058.63 | 906.06 | 803.01 | 727.58 | 622.72 | 551.90 |
| 127.00 | 128.19 | 3470.08 | 2384.97 | 1915.22 | 1639.19 | 1452.78 | 1316.32 | 1126.59 | 998.49 |
| 152.40 | 154.05 | 5618.86 | 3861.82 | 3101.16 | 2654.21 | 2352.38 | 2131.42 | 1824.21 | 1616.76 |

## 7. VENTING OF GAS SUPPLY REGULATORS

AERCO's general guidelines for venting of gas regulators are listed below. AERCO requires that these guidelines be followed to ensure the most reliable and proper operation of AERCO gas fired equipment. It is also required that you consult local codes and the gas regulator manufacturer for additional details. Always follow the most stringent guidelines available, including those listed below.

- When venting a gas supply regulator, the vent pipe must be no smaller than the regulator vent size.
- In a multiple unit installation, each regulator must have a separate vent line.
- Vent lines must not be manifolded together or with any other equipment at the site that also requires atmospheric vents.
- When sizing the vent, pipe diameters must be increased by one pipe diameter every 20 equivalent feet of pipe.

Each $90^{\circ}$ elbow is equivalent to approximately:
$\Rightarrow 2.5$ feet ( 0.76 m ) for nominal pipe sizes of up to $3 / 4^{\prime \prime}$ ( 19 mm )
$\Rightarrow 4.5$ feet $(1.37 \mathrm{~m})$ for nominal pipe sizes of up to $1-1 / 2^{\prime \prime}(38 \mathrm{~mm})$
$\Rightarrow 10.5$ feet $(3.2 \mathrm{~m})$ for nominal pipe sizes of up to $4^{\prime \prime}$ ( 101 mm )

Each $45^{\circ}$ elbow is equivalent to approximately:
$\Rightarrow 1$ foot ( 0.3 m ) for nominal pipe sizes of up to $3 / 4^{\prime \prime}$ ( 19 mm )
$\Rightarrow 2$ feet $(0.61 \mathrm{~m})$ for nominal pipe sizes of up to $1-1 / 2^{\prime \prime}(38 \mathrm{~mm})$
$\Rightarrow 5$ feet $(1.52 \mathrm{~m})$ for nominal pipe sizes of up to $4^{\prime \prime}$ ( 101 mm )

Change Log

| Date | Description | Changed by |
| :---: | :--- | :--- |
| $6 / 27 / 2023$ | Rev. A Initial Release | D. Barron |
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